

METHOD FOR SIMULTANEOUSLY ABATING NITRIC OXIDES AND NITROUS OXIDES IN GASES CONTAINING THEM

CROSS REFERENCE TO RELATED APPLICATIONS:

The present application claims the benefit of International Application
5 PCT/FR00/00367 filed February 15, 2000, and French patent Application
FR99/01999, filed February 18, 1999, the disclosures of both of which are hereby
incorporated by reference.

BACKGROUND OF THE INVENTION:

(i) Field of the Invention

The present invention relates to the area of protection of the environment. It
relates to the purification of industrial gas prior to their release to the atmosphere.
More specifically, it relates to the treatment of effluent tail gases coming from nitric
acid factories that typically contain, besides oxygen at the rate of 1.5 to 5%, from 0.5
% to 5% water, from 50 to 6000 ppmv of nitric oxides and from 500 to 1500 ppmv of
15 N_2O , wherein the temperature is generally less than 400 °C.

(ii) Description of Related Art

The nitric oxides NO_x , which include NO and NO_2 , are polluting gases,
principally by reason of their corrosive action. They are for the most part the cause
of acid rain. In the synthesis of nitric acid, they are the gases that are produced by
20 oxidation of ammonia by oxygen over platinum at high temperature. They are
retained in absorption towers by being transformed there to nitric acid. They escape
in the tail gases, where it is known to eliminate them to a suitable level by catalytic
ammonia reduction: it is the process called SCR (denoting selective catalytic

reduction), which is implemented thanks to zeolitic catalysts. European patent (EP-B-0393917, Engelhard Corporation) reveals that the beta zeolite associated with iron as promoter, is an effective catalyst for the selective reduction of NO_x by ammonia; it makes no reference to nitrous oxide

5 Nitrogen protoxide or nitrous oxide, of formula N_2O is likewise produced at the time of the oxidation of ammonia by air oxygen at high temperature, and it also is produced during the SCR destruction of nitric oxides. For a long time, one hardly worried about eliminating it before release to the atmosphere until an awareness developed that it was a gas having a strong greenhouse effect. Japanese patent JP 10 08057262 (Babcock Hitachi) recommends the use of beta-iron for bringing down nitrous oxide by reduction with ammonia. The inventor does not refer to the NO_x oxides.

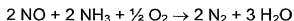
15 The use of a series of catalytic pots in the same installation in order to successively reduce the content of NO_x and N_2O gases is a solution of little satisfaction industrially. There has therefore been sought a unique catalyst which would simultaneously carry out the destruction of NO_x and N_2O by ammonia and, under the same operating conditions, in particular at a temperature less than 400°C , which besides has a hydrothermal stability sufficient at 600°C to resist temperature periods to which it can be subjected under certain circumstances of its use. An SCR 20 catalyst which in a single operation would permit lowering at the same time of all of the nitrogen oxides and , the protoxide such as the acid oxides, would represent a highly appreciated technical advancement. The idea therefore came to the inventors to inquire whether beta-iron would not be the ideal catalyst for such a treatment,

despite the well founded prejudice according to which the ammonia SCR catalysts have only the tendency to manufacture nitrous oxide.

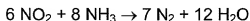
SUMMARY OF THE INVENTION:

It has thus been discovered that at the same time one could destroy N₂O and NO_x in gases which contain them as well as oxygen by selective catalytic reduction by ammonia over beta zeolite containing iron (hereinafter FeBEA). The possible reactions of ammonia and of the nitrogen oxides are multiple.

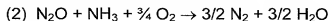
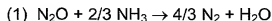
For the reaction NO/NH₃, one probably has:



For NO₂/NH₃, one would have:



For N₂O/NH₃, it was detected by ¹⁵NH₃ nuclear magnetic resonance that two reactions took place:



The system is therefore one of high stoichiometric complexity, but it can be proposed that the optimal operating conditions of the invention are found when the ammonia is present in a ratio of 0.7 and 1.7 with respect to the nitrogen oxides. The conversions of N₂O and of NO_x are thus total. The leakage of ammonia is non-existent, which is consistent with the known property of iron-zeolites as being excellent catalysts for the oxidation of NH₃ to N₂, to the extent that the oxygen is

present in sufficient quantity. The values 0.7 and 1.4 however are not absolute boundaries. It was simply desired to point out that in reasonable borderline cases, for example a gaseous mixture containing as nitrogen oxide only some NO, the NH₃/nitrogen oxides ratio although equal to 1 in theory for an ideal stoichiometry conversion is often observed with the value 0.7; that as far as the upper boundary is concerned, the richest reaction in NH₃ is the reduction of the NO₂, and that for a mixture that would contain only NH₃ and NO₂, the ratio would be 8/6. For high NH₃/nitrogen oxide ratios (greater than 1.4), the elimination of the nitrogen oxides also remains quite effective and the ammonia is equally consumed but for nothing. Stoichiometric ratios greater than 1.4 are not of industrial interest. In the case of a classical gas mixture coming out from a nitric acid production factory, the NH₃/nitrogen oxides ratio ranges in the vicinity of 0.9.

DETAILED DESCRIPTION OF PREFERRED EMBODIMENTS:

The synthesis of beta-zeolite (BEA) was described in 1967 by Wadlinger R.L. et al. (R.L. Wadlinger, G.T. Kerr and E.J. Rosinski, 1967 in US 3,308,069), and its structure was elucidated independently towards 1988 by Newsam J.M. and coll. (Proc. R. Soc. Lond. A 420, 1588) and Higgins J.B. and coll. (Zeolites, 8, 446, 1988). It is a zeolite which results from the intergrowth of two distinct but intimately bound polytypes, one of tetragonal symmetry (polytype A), the other of monoclinic symmetry (polytype B), both constructed starting from the same centrosymmetric tertiary unit and possessing tridirectional systems of pores formed from 12 tetrahedron cycles. The canals are open, (0.64 X 0.76 nm) and (0.55 X 0.55 nm) (see W.M. Meier and D.H. Olson, Zeolites, 12 (1992) 459-654). The corresponding

structure is visualizable on the internet at <http://www.iza-sc.ethz.ch/iza-SC/>. It is with the faujasite, one of the most open porous systems among the zeolites.

The beta zeolite of the invention is a BEA in which the Si/Al ratio ranges between 8 and 100, preferably between 8 and 20. It contains iron, and its iron content goes from 0.02% to 8% (by weight).

It is of little importance, it seems, whether the iron be brought by impregnation or by exchange, the resulting solid showing a comparable efficacy in the transformation of N_2O to N_2 . It is the iron exterior to the grains or present in the canals or the crystal cages which is the active iron. The iron that is incorporated in the network during the zeolite synthesis is in tetrahedral coordination and does not obtain any catalytic activity. It is necessary that there be a minimum (0.02%) of non-tetrahedral iron in the catalyst for it to express its useful properties in the invention. The upper amounts are limited to 8% in a somewhat arbitrary fashion, although the elevated iron contents do not stand in the way of the operation of the catalyst; they are without real industrial interest. Amounts comprising between 0.5 and 3% will be preferred. The catalyst of formula $Fe(79)BEA_n$ of example 1a) and of figure 3a with an iron content of 1.50% seems to effect a valid optimum. The impregnation technique is reserved for the FeBEA strongly charged with iron.

Exchange and impregnation are techniques well known to a person skilled in the art and their application to beta zeolite does not give rise to any major problem. In order to prepare an iron beta-zeolite by exchange, iron is introduced, via the solution of one of its hydrosoluble salts, either in a BEA under its typical form, which is that of a partially soda BEA, or in a BEA put beforehand under ammonium form by

pre-exchange by NH_4^+ which is preferably carried out in order to eliminate Na traces and to obtain a catalyst of slightly higher performance for reduction of nitrogen oxides. These techniques provide powder zeolites.

The catalysts according to the invention are in a rather agglomerated form, a preferred form in industrial practice for reasons of minimizing the loss of gas charge at its passing through of the catalyst bed. The agglomeration of the zeolites is well known to a person skilled in the art. One proceeds by binding together the zeolite powder with a binding agent generally fluidified by water, often comprised of a clay which is at the same time sufficiently plastic to be able to form the agglomerate into setting balls, pastilles by molding or threads by a spinning press, and hardenable by firing in order to provide sufficient cohesion and hardness to agglomerate it. The clays used are kaolinites, attapulgites, bentonites, a halloysite or mixtures of these clays. There can also be used siliceous or aluminous binders. In particular the agglomeration with peptized aluminas gives very resistant granules, this way of agglomeration being possible here because the BEA is not degraded by the acidity of the binder.

After agglomeration, the granules are thermally activated. It is understood that they are subjected to a firing carried out under air, at a temperature of about 400 °C, the role of the firing being at the same time to harden the binder, to dehydrate it without hydrothermally degrading it, and in the case of the BEA exchanged starting from an ammonium form, to eliminate a large part of the ammonium ions and to put the zeolite under H form.

One can equally start by agglomerating the partially soda BEA, then hardening it by calcination, and proceeding to the exchanges on the agglomerate. After drying, a second calcination permits putting the BEA/iron under H form if the BEA made use of was taken under ammonium form.

The process of gas treatment according to the invention comprises passing the gas to be purified, of which the range of concentrations of nitrogen oxides, N_2O and NO_x flowing together, extends from 100 to 7000 ppmv, and which besides contains from 1.5 to 5% oxygen and 0.5 to 5% water, (N_2O extending from 50 to 5000 ppm and NO from 50 to 2000 ppm), across a catalyst bed disposed in a reactor maintained at a temperature ranging between 200 and 600 °C, at voluminal output velocities per hour (VVH) of 1000 to 50 000 h^{-1} . The reactor charged with the FeBEA catalyst bed can be an axial or radial flux reactor. The corresponding technology hardly differs from that of the SCR except for replacing the classical catalyst with the BEA-iron based catalyst.

The BEA-iron system was confirmed to be the best system for the conversion of the nitrous oxide, if it is compared to other proposed zeolites of varying recoveries as nitrogen oxide reduction catalysts, such as mordenite-iron or the Y-iron zeolites.

EXAMPLES

In all of the examples provided, the exchange rate (%) of iron was defined as follows: 3 times the molar iron content divided by the molar aluminum content and multiplied by 100. Subsequently, a writing such as Fe(Z)BEA will represent an FeBEA in which the iron exchange rate is Z%.

Example 1: preparation of FeBEA powders by exchange

The BEA zeolite used is the CP814E powder provided by Zeolyst international (PQ corporation). Its $\text{SiO}_2/\text{Al}_2\text{O}_3$ ratio is about 25; it contains 0.05% by weight of Na_2O . Its specific surface is about $680 \text{ m}^2/\text{g}$. This zeolite exhibits X diffraction lines characteristic of a BEA zeolite, such as reported in appendix II of volume 10 of the review Zeolites (1990) and in the article by J.B. Higgins (Zeolites, vol. 8 (1988) 446-452).

1a) Preparation of FeBEA by simple exchange

The following FeBEA_e solids were prepared (the index e qualifies the introduction of the iron by an exchange process).

Fe(5)BEA_e

Fe(10)BEA_e

Fe(24)BEA_e

Fe(49)BEA_e

Fe(79)BEA_e

by mixing 2 g of BEA zeolite powder (PQ CP814E) with 500 cm^3 of an aqueous $\text{Fe}(\text{NO}_3)_3$ solution (0.159 g of $\text{Fe}(\text{NO}_3)_3$, by leaving the mixture under agitation for 24 h, then by separating the solid phase from the liquid phase by centrifugation; by then washing the solid thus prepared with 200 ml of water at $\text{pH} = 5$, by centrifuging it again, drying it at 80°C for 12 hours under air, then calcining it at 500°C for 24 hours. A powder is obtained which is shown to have the composition of a Fe(49)BEA_e.

By varying the quantity of ferric solution, other compositions Fe(5)BEA_e, Fe(10)BEA_e, Fe(24)BEA_e, Fe(79)BEA_e were obtained. The respective compositions are:

Fe(5)BEA_e, with by weight Si=36.4%, Al=2.67%; Na=0.52%, Fe=0.11%;
 Fe(10)BEA_e, with by weight Si=35%, Al=2.64%; Na=0.39%, Fe=0.19%;
 Fe(24)BEA_e, with by weight Si=34.7%, Al=2.43%; Na=0.57%, Fe=0.40%
 Fe(49)BEA_e, with by weight Si=35.45%, Al=2.65%; Na=0.75%, Fe=0.90%;
 Fe(79)BEA_e, with by weight Si=34.7%; Al=2.75%; Na=0.50%; Fe=1.50%.

1b) Preparation of FeBEA powder with ammonium pre-exchange

There were mixed 2 g of BEA (PQ CP814E) with 200 cm³ of a 2M solution of NH₄NO₃ and the mixture brought to reflux for 24h. The solid phase is then washed with exchanged water and dried at 80 °C to give NH₄-BEA_a (the index a qualifies the double ammonium exchange).

There were mixed 2 g of this NH₄-BEA with 500 cm³ of an aqueous Fe(NO₃)₃ solution (0.159 g of Fe(NO₃)₃) and the mixture is left under agitation for 24 h, after which the solid phase is separated from the liquid phase by centrifugation. The solid is washed with 200 ml of water at pH = 5. The mixture is again centrifuged and the solid is first dried at 80°C for 12 hours under air then calcined at 500 °C for 24 hours. A powder is obtained which is shown to have the composition of a Fe(49)BEA_a with by weight Si=35.6%, Al=2.8%, Na=<0.05%, Fe=1%.

Example 2: preparation of iron beta-zeolite powder by impregnation of the iron salt.

The following FeBEA solids were prepared (the index i qualifies the introduction of the iron by an impregnation process):

Fe(51)BEA_i
 Fe(126)BEA_i
 Fe(169)BEA_i
 Fe(330)BEA_i

by impregnation of the BEA (PQ CP814E) zeolite according to the following operative process.

There is impregnated 2 g of BEA with 20 ml of three aqueous solutions of $\text{Fe}(\text{NO}_3)_3$ containing respectively 0.130; 0.389; 0.519; 1.038 g of $\text{Fe}(\text{NO}_3)_3$. The solid is then dried at 80 °C then calcined under air at 500 °C.

Powders are obtained which are shown in analysis to have the composition of:

- Fe(51)BEA_i, with by weight Si=33.0%, Al=2.85%; Na=0.70%, Fe=1.00%
- Fe(126)BEA_i, with by weight Si=33.5%, Al=2.70%; Na=0.55%, Fe=2.35%
- Fe(169)BEA_i, with by weight Si=33.0%, Al=2.75%, Na=0.50%, Fe=3.20%
- Fe(330)BEA_i, with by weight Si=32.6%, Al=2.60%; Na=0.85%, Fe=5.25%.

Example 3: Reduction of the N₂O- Comparative efficacy of various zeolites

(Fig 1)

The efficacy of the Fe(49)BEA_e was compared to other iron zeolites wherein the introduction of the iron was carried out by exchange according to the process described in example 1 without passing by the ammonium pre-exchange (Y-iron, Mordenite-iron, ZSM5-iron). The examples that follow make reference to catalytic tests at programmed temperature. The present profiles were obtained under variable conditions, but wherein the common points are here expressed:

- temperature evolution from 25 to 550 °C, at the rate of 5 °C per minute, or a test at temperature stages descending from 550 to 25 °C, with 1 hour stages every 10°C.
- detection and analysis of the gas effluents are carried out with the help of a quadropolar type mass spectrometer (QMS 200 of Balzers);

- the catalyst sample (75 mg) is first activated at 550 °C for an hour after climbing in temperature at the rate of 10 °C per minute in air (flow rate 30 cm³.min⁻¹);

the gaseous mixture to be purified comprises from 3% O₂, 0-2000 ppmv N₂O, 0-4000 ppmv NH₃, 0-1000 ppmv of NO, 0-3% H₂O, in helium whose flow rate varies so as to correspond to VVHs varying from 10000 h⁻¹ to 35000 h⁻¹.

A 50% conversion is achieved at 365 °C for FeBEA whereas temperatures of 430 °C, 430 °C and 500 °C are necessary for the Fe-ZSM5, Fe-MOR and Fe-Y zeolites respectively. This figure shows that the N₂O conversion profile of the FeBEA is shifted between 50°C and 140°C towards low temperatures, according to the conversion, as compared to other iron zeolites. This result confirms that the iron beta zeolite is the most active in eliminating N₂O in the presence of ammonia.

Example 4: Influence of the ammonia content on the N₂O reduction (Fig. 2a)

The effect of the ammonia concentration in reduction in N₂O programmed temperature was carried out in the presence of Fe(49)BEA₆ under the following conditions: 2000 ppmv N₂O, 1333 to 3500 ppmv NH₃, 3% O₂ and a voluminal velocity per hour of 35000 h⁻¹.

In the absence of ammonia, the iron beta zeolite is hardly active in eliminating N₂O. A NH₃/N₂O ratio =0.9 (1800 ppm NH₃, 2000 ppm N₂O) seems necessary in order to achieve satisfactory conversions (>80%). Too high an ammonia concentration (ex. 3500 ppm, NH₃/N₂O=1.75) renders the reductant activity of the iron beta-zeolite less effective.

Example 4 bis: Influence of the ammonia content on the simultaneous reduction of N_2O and NO (Fig. 2b)

The effect of the ammonia concentration in reduction in programmed temperature of an N_2O , NO mixture was carried out in the presence of $Fe(49)BEA_6$ under the following conditions: 2000 ppmv N_2O , 500 ppmv NO, 1333 to 3500 ppmv NH_3 , 3% O_2 and a voluminal velocity per hour of $35000\ h^{-1}$.

The evolution of the N_2O content can be read in figure 2b1 and that of the NO content in figure 2b2. As far as the conversion of N_2O is concerned, it is noted as in the case of N_2O alone that a NH_3 /nitrogen oxides ($N_2O + NO$) ratio=0.8 (2000 ppmv NH_3 , 2000 ppmv N_2O , 500 ppmv NO) is necessary in order to achieve satisfactory conversions (>80%). It can also be noted that under inferior stoichiometric conditions (NH_3 /nitrogen oxides <0.8), the ammonia permits preferential consumption of NO, the N_2O no longer being destroyed even when in the remaining proportions of ammonia. As far as conversion of NO is concerned, too high an excess of NH_3 ($NH_3/NO=8$, 4000 ppmv NH_3 , 500 ppmv NO) strongly diminishes the efficacy to reduce NO, but all the excess NH_3 introduced is transformed to N_2 .

Example 5: influence of the beta-iron iron content

The effect of the iron content of the beta-zeolite was analyzed by programmed temperature reduction of N_2O (Fig. 3a) of NO (Fig. 3b) and of a N_2/NO mixture (Fig. 3c) under the following conditions: 2000 ppmv N_2O , 2000 ppmv NH_3 , 3% O_2 ; 2000 ppmv N_2O , 2000 ppmv NH_3 , 3% O_2 , 1500 ppmv N_2O , 1000 ppmv NO, 2000 ppmv NH_3 , 3% O_2 , 2% H_2O and a voluminal velocity per hour of $35000\ h^{-1}$.

It is observed that an exchange rate ranging between 25 and 79% permits obtaining the best activity at the lowest temperature.

Example 6: influence of the method of iron introduction (Fig. 4)

The nature of the way of introducing iron into the Beta-zeolite was examined by
5 programmed temperature reduction of N_2O under the following conditions: 2000
ppmv N_2O , 2000 ppmv NH_3 , 3% O_2 and a voluminal velocity per hour of $10000\ h^{-1}$.

Regardless of what the technique is for introducing iron, FeBEAs are obtained
having comparable efficacy in the transformation of N_2O to N_2 .